## SUPPLEMENTARY FILE

## **Optimization of Spray Drying Process in Microencapsulated Cream Powder**

## Production

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Supplementary Table 1. Results of statistical analysis for verification of optimization of microencapsulated cream powder production.

Response	Predicted Values	Experimental Values <sup>†</sup>	SE <sup>‡</sup>	Difference	%Error <sup>§</sup>	<i>P</i> -value
Yield (%)	36.37	$35.31 \pm 1.67$	0.749	-1.06	3.01	0.229
Bulk Density (kg/m <sup>3</sup> )	269.9	$270.5\pm5.4$	2.396	0.6	0.21	0.821
Wettability (s)	115.2	$119.6\pm12.0$	5.354	4.4	3.68	0.457
Surface Fat (%)	26.20	$26.52\pm0.36$	0.159	0.32	1.21	0.115

<sup>†</sup>Experimental values were expressed as mean  $\pm$  standard deviation.

<sup>‡</sup>Mean standard error.

 ${}^{\$}\%Error = \frac{\left|y_{exp} - y_{pre}\right|}{y_{exp}} \times 100$ 

Physical Properties		Free Fatty Acid Composition (mg/100 g fat)			
Water Activity	$0.175\pm0.006$	Butyric acid (C <sub>4:0</sub> )	$2.92\pm0.28$		
Solubility (%)	$51.7\pm0.6$	Caproic acid (C <sub>6:0</sub> )	$1.90\pm0.06$		
Tapped Density (kg/m <sup>3</sup> )	$483.2\pm9.5$	Caprylic acid (C <sub>8:0</sub> )	$2.07\pm0.09$		
$HR^1$	$1.79\pm0.01$	Capric acid (C <sub>10:0</sub> )	$5.42\pm0.28$		
$CI(\%)^2$	$44.0\pm0.3$	Lauric acid (C <sub>12:0</sub> )	$7.56\pm0.34$		
Particle Density (kg/m <sup>3</sup> )	$1150.0\pm50.1$	Myristic acid (C <sub>14:0</sub> )	$24.34 \pm 1.11$		
Color Properties <sup>3</sup>		Palmitic acid (C <sub>16:0</sub> )	$125.0\pm 6.3$		
L	$95.05\pm0.05$	Stearic acid (C <sub>18:0</sub> )	$57.54\pm8.19$		
A	$\textbf{-0.16} \pm 0.01$	Oleic acid (C <sub>18:1</sub> )	$119.0\pm9.4$		
В	$7.53\pm0.04$	Linoleic acid (C <sub>18:2</sub> )	$11.88 \pm 1.20$		
Chroma	$7.53\pm0.04$	Linolenic acid (C <sub>18:3</sub> )	$1.90\pm0.11$		
BI	$7.94\pm 0.04$	VFFA <sup>4</sup>	$12.31\pm0.47$		
ΔE-cream	$77.88 \pm 0.05$	MLCFFA <sup>5</sup>	$347.2\pm17.5$		
$\Delta E$ -emulsion	$54.92\pm0.05$	$\mathrm{TFFA}^{6}$	$359.5 \pm 17.7$		

Supplementary Table 2. The physical properties and free fatty acid composition for the microencapsulated cream powder produced at optimum spray drying conditions.<sup>†</sup>

<sup>†</sup> Experimental values were expressed as mean  $\pm$  standard deviation.

<sup>1</sup> HR: Hausner Ratio

<sup>2</sup>CI: Carr Index

<sup>3</sup> L: lightness; a: redness/greenness; b: yellowness/blueness;  $\Delta E$ -cream: color difference with cream as reference;  $\Delta E$ -emulsion: color difference with emulsion as reference; BI: Browning Index

<sup>4</sup> VFFA: Total volatile free fatty acids (C<sub>4:0</sub>-C<sub>10:0</sub>) <sup>5</sup> MLCFFA: Total medium- and long-chain fatty acids (C<sub>12:0</sub>-C<sub>18:3</sub>)

<sup>6</sup> TFFA: Total free fatty acids



**Supplementary Fig. 1.** Response surface and contour plot for the effects of inlet temperature and aspiration rate on the bulk density at constant feed flow rate (19.50 mL/min).



**Supplementary Figure 2.** Response surface and contour plot for the effects of feed flow rate and aspiration rate on the bulk density at constant inlet temperature (170 °C).



**Supplementary Figure 3.** Response surface and contour plot for the effects of inlet temperature and aspiration rate on the wettability at constant feed flow rate (19.50 mL/min).



**Supplementary Figure 4.** Response surface and contour plot for the effects of inlet temperature and feed flow rate on surface fat at constant aspiration rate (75%).



**Supplementary Figure 5.** Response surface and contour plot for the effects of feed flow rate and aspiration rate on surface fat at constant inlet temperature (170 °C).



**Supplementary Figure 6.** Contour plot for the effects of inlet temperature and feed flow rate on desirability function of the optimization process at constant aspiration rate (75%).



**Supplementary Figure 7.** Contour plot for the effects of inlet temperature and aspiration rate on desirability function of the optimization process at constant feed flow rate (19.50 mL/min).



**Supplementary Figure 8.** Contour plot for the effects of feed flow rate and aspiration rate on desirability function of the optimization process at constant inlet temperature (170 °C).



Supplementary Figure 9. Scanning electron micrographs of powder particles dried at optimum

spray drying conditions. The magnifying ratios were 1000x (a), 2500x (b), and 5000x (c).